

### Webinar Presentation: ION's Battery Recycling PFS

**Iondrive Limited (ASX: ION) (Iondrive or the Company)** is pleased to provide a copy of the presentation being provided at a Webinar commencing today at 12pm AEDT. At the webinar, the Company's CEO, Dr Ebbe Dommisse, will present the Company's latest developments following the finalisation of the PFS activities for its DES battery recycling technology.

Authorised for release by the Board of Iondrive Limited.

### **Further Information**

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### **Iondrive Limited: Company Profile**

Iondrive is an emerging leader in battery recycling technology, listed on the Australian Securities Exchange (ASX ticker "ION"). The company's primary focus is on developing and commercialising innovative solutions for lithium battery recycling. Iondrive's Hydrometallurgical Battery Recycling project employs a patented, environmentally safe solvent to gently separate critical components from used batteries, providing a safer and more efficient alternative to traditional methods.

In addition to its battery recycling initiatives, londrive holds exclusive worldwide licenses from the University of Adelaide for next-generation battery technologies, including an enhanced performance non-flammable lithiumion based battery and a low-cost, high cycle life water-based battery.

While the main emphasis is on battery technology, londrive also maintains a portfolio of exploration projects in South Korea, focusing on lithium. Backed by a first-class technical team, londrive is dedicated to advancing sustainable battery technologies and contributing to the circular economy in both Europe and Australia.

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**INVESTOR WEBINAR:** 

# Pre-Feasibility Study – Greener and Cheaper Battery Recycling Technology

November 2024



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The Company recommends that this presentation is read in conjunction with its relevant ASX Announcements – in particular the announcement of 1 November 2024

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# 01

# Background





# Powering the Future of Sustainable Battery Recycling



### Huge Market Opportunity

- minerals to be sourced from recycling by 2030.

### Innovative, Green Technology

- from lithium-ion batteries.
- methods.

### **Positive Trial Results & De-Risking**

- results, confirming the DES process's commercial potential.
- Pre-Feasibility Study completed October 2024.

### **Strong Industry Partnerships**

demands for battery recycling and sustainable practices.

### Well-Funded for Growth with Strong Support from Key Investors

Strata Investment Holdings and Ilwella Pty Ltd, positioning the company to prepare for the Pilot Plant stage.





• Global battery recycling demand is forecast to grow 25% annually, reaching 11 million tonnes of black mass by 2040. • EU regulatory tailwinds, including the Batteries Regulation, will drive demand for recycled materials, requiring 25% of critical

• Iondrive's patented Deep Eutectic Solvent (DES) process offers an environmentally friendly solution to extract critical minerals

• The DES process minimises toxic waste, reducing both environmental impact and operating costs, compared to traditional

• Large-scale trials at the University of Adelaide and independent validation by IMO Perth show high recovery rates with scalable

• Collaboration with PEM RWTH Aachen University to commercialise recycling technology in Europe, aligning with EU regulatory

• Iondrive is well-capitalised with \$3M in the bank (30 Sept + RDTI received Oct) and strong backing from cornerstone investors,





## **Commercialisation Pathway**





02

# PFS Update





# **DES Development Pathway**



## **PFS OBJECTIVES**

- Techno-Economic Evaluation: Technical Feasibility and Economic Viability of DES process
- Decision Point: Go/No Go gate for progressing to Pilot Plant stage





# **PFS De-risking Activities**

Iondrive has **completed** the Pre-feasibility Study on Schedule in **October 2024.** The PFS is a **Techno-Economic Evaluation** focusing on technological, commercial, and executional de-risking strategies. These de-risking activities ensure a strong foundation for successfully executing the commercialisation pathway for our recycling technology.

### Technology

- V
  - Process Technology Review (Lycopodium)
  - Large-scale bench trials and 3<sup>rd</sup> party validation trials (**IMO**)
- High-level process engineering design of 10,000 tpa black mass plant (Wood)
- Value Engineering + Solvent Recovery (Koch Modular)
- Cost estimation Capex/Opex (Wood)





In Progress

Pending ()





# 03

# Technology De-Risking





# Large-scale Trials

### Ba

attery Minerals		Total Recovery						
	Pretreated Black Mass	Raw Black Mass	IMO <sup>1</sup> pCAM	UoA pCAM				
Lithium	89.1%	82.9%	NA	NA				
Nickel	100.0%	88.5%	98.3%	97.6%				
Cobalt	98.6%	96.5%	98.6%	97.6%				
Manganese	98.4%	94.4%	84.6%	87.7%				

## **Key Insights**

- New Pre-treatment process Removes impurities very well & improves Robustness for mixed black mass •
- Very high Total Recoveries vs. Conventional hydromet processes lacksquare
- <sup>1</sup> Independent 3'd party validation (IMO, Perth) lacksquare
- <2% Solvent Losses highlighting efficiencies ullet
- Proof that the Chemistry Scales supporting commercial development ullet

# **Engineering Studies**

### Wood Concept Study<sup>a</sup>

- treatment stage).
- Capex and Opex estimations are within  $\pm 50\%$ , indicating competitive positioning.
- Noted advantage: "*londrive showing the competition tail lights*," according to Wood.

### Koch Modular Concept Study<sup>b</sup>

- Specific focus on Solvent Recoveries
- Developed a Process Flowsheet to +99% purities (if required)
- Confirmed technically feasible Process Configuration
- Capex estimations  $(\pm 50\%)$

<sup>b</sup> Koch Modular PFS Report (internal report)

**Salondrive** 

Designed for 18,000 tpa raw black mass, yielding 10,000 tpa treated black mass with battery-grade materials. Utilises inputs from large-scale bench trials to develop a Process Flowsheet targeting 99% purity (excl. pre-

<sup>&</sup>lt;sup>a</sup> Wood PFS Report (internal report)



# Conclusions

- Chemistry Scales
- Higher metals recoveries than conventional hydromet
- High solvent recoveries with environmentally acceptable solvents •
- **Technically Feasible** •
- Capex and Opex highly competitive
- Now an engineering challenge to design a commercially viable process •
- Next Steps: ullet
  - Pilot Plant to progress: •
    - TRL 4 to TRL 6
    - Batch to Continuous Integrated process
    - Reflective of commercial operation
  - Wood Concept Study for Pretreatment Process







# **Commercial De-Risking**

# PEM Benchmarking Study<sup>c</sup>

### Objectives

**S**alondrive

- in EU
- Comparison of Capex and Opex (WOOD Study vs PEM's database), and Revenues  $\bullet$

### **Results**<sup>d</sup>

ltem	ION DES	ION DES +30% <sup>1</sup>	Competition	ION 2035
Revenue	€7,158/t	€7,158/t	€6,489/t	€15,132/t
Opex <sup>2</sup>	€4,096/t	€4,981/t	€4,667/t	€4,096/t
EBITDA <sup>2</sup>	€3,061/t	€2,177/t	€1,822/t	€11,036/t
Capex	€10,144/t	€12,911/t	€20,218/t	€10,144/t

- Normalised to €/tonne black mass  $\bullet$
- Assuming a +30% increase<sup>d</sup> in Capex and Opex to allow for Pretreatment Plant  $\bullet$
- <sup>2</sup> Excluding cost of black mass lacksquare
- lacksquare
- DES Process' Sales Revenue higher than competition (product mix)  $\bullet$

<sup>c</sup> PEM Aachen University PFS Report (internal report)

<sup>d</sup> ION internal economic modelling to be updated with 3'd party independent modelling

Evaluation of ION's DES process economics with a similar-sized conventional hydromet LiB recycling process

ION's DES Process very competitive on Capex and parity on Opex for Pretreatment Process included



# Conclusions

- at parity.
- profitability expected to grow as commodity prices rise.

## Next Steps:

- scenarios.
- product and black mass pricing.

• **Commercial Competitiveness**: Capex is 36% lower than competitors, with Opex

• **Profitability**: The DES process is more cost-effective than EU competitors, with

Independent third-party economic modelling to assess NPVs and IRRs across

Develop future pricing models using Benchmark Minerals Intelligence for both





# 05 PFS Conclusions







# Strategic Industry Partnerships – De-Risking Strategy

We are forming strategic partnerships to DE -RISK commercialisation (PEM Motion)

### TOP 10 REASONS FOR STARTUP FAILURE

No market need Ran out of cash Not the right team Get outcompeted Pricing/cost issues Poor product Need/lack business model Poor marketing Ignore customers Product mistimed



### **DE-RISK INVESTMENT DECISIONS**

42%



Market Competitiveness

Technology Innovation



Product Scalability



Team Experience



**Customer Demands** 



**Regulatory Requirements** 





# **PFS CONCLUSIONS – Greener and Cheaper**

## TECHNOLOGY

- DES Process shown to be **Technically Feasible**
- **Compelling Environmental Value Proposition**

## COMMERCIAL

- Benchmarking showed that DES process is **Commercially Viable** and **Competitive** (Capex + Opex vs competition)
- **Increasing Profitability** over time with commodity price increases

## MARKET

- early mover to capture market share before anticipated consolidation
- early mover advantage
- PEM Consortium the breakthrough to establish foothold in EU market

**Salondrive** 

ISO 56,000 Dashboard	Score
Feasibility (Technology)	High
Viability (Commercial)	High
Desirability (Market)	High

Rho Motion Study highlighted the **Attractiveness of the EU Market** for novel process for battery recycling PEM Competitor Analysis showed detailed landscape of competitors in EU and concluded that advantage for

Industry Partnerships with PEM and TNO underlining the attractiveness of DES Technology in EU to secure



## Next Steps

- Proceeding to Pilot Plant stage •
- Wood Concept Study for Pretreatment Process ullet
- Independent Economic Modelling to develop NPVs and IRRs to evaluate Business Case(s) for • scenarios
- Pursuing non-dilutive Funding grants etc in AUS + EU (noting that backed by strong investor) support)

# **Pilot Plant Development Schedule**

Nov-24	Dec-24	Jan-25	Feb-25	Mar-25	Apr-25	May-25	Jun-25	Jul-25	Aug-25	Sep-25	Oct-25	Nov-25	Dec-25
Stage 1													
		Stage 2											
									Sta	ge 3			

Stage 1: Pilot Plant preparatory experiments Stage 2: Pilot plant semi-continuous unit operations Stage 3: Integrated continuous Pilot Plant